

# Soot Oxidation with Ir-based Catalysts in the Presence of O<sub>2</sub> and NO

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**Abstract** The soot oxidation with Ir-based catalysts was investigated using simulated diesel exhaust gases. By comparing with Pt/SO<sub>2</sub>, Ir/SO<sub>2</sub> showed similarly catalytic activity and high CO selectivity. The effect of Ir content on the catalytic activity and CO selectivity was examined. With the increasing of Ir content in the range examined ( from zero to 5% ), the catalytic activity increased and the CO selectivity decreased. Furthermore, the effect of support oxides was obtained: the catalytic activity was Ir/ZSM-5 > Ir/SO<sub>2</sub> > Ir/ $\gamma$ -Al<sub>2</sub>O<sub>3</sub> and the CO selectivity was Ir/ZSM-5 < Ir/ $\gamma$ -Al<sub>2</sub>O<sub>3</sub> < Ir/SO<sub>2</sub>.

**Key words** soot oxidation; Ir-based catalysts; NO

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## 1 Introduction

Soot emitted from diesel engines causes a serious problem to human health and environment. The use of a catalyst is the most preferential way to promote soot oxidation at exhaust gas temperature. During the past decade, many catalytic systems have been researched<sup>[1-3]</sup>. Among them, the Pt-based catalysts exhibit a high level of catalytic activity. However, this system that obviously does not remove NO is blamed for the increase in the NO<sub>2</sub> concentration in the exhausts.

In our research, we are interested in Ir-based catalysts for soot oxidation, since they show high catalytic activity for NO reduction with CO in the presence of excess oxygen<sup>[4-5]</sup>. It is well known that soot oxidation is an important source to produce CO. If we can control soot to oxidize to CO and then use this CO to reduce NO to N<sub>2</sub>, we will realize to simultaneously remove the soot and NO. Thus, the aim of this work is to investigate the catalytic activity and CO selectivity of Ir-based catalysts for soot oxidation using simulated exhaust gases, including O<sub>2</sub> and NO.

## 2 Experimental

The supported catalysts were prepared by incipient wetness impregnation method with the solution of H<sub>2</sub> PtCl<sub>6</sub> · 6H<sub>2</sub>O and H<sub>2</sub> PtCl<sub>6</sub> · 6H<sub>2</sub>O. Catalytic activity for soot oxidation was measured with temperature pro-

grammed reaction ( TPR ) system. The catalytic activity was evaluated at the initial temperature ( T<sub>i</sub>, the temperature when the CO + CO<sub>2</sub> concentration reached 100 ppm ). The CO selectivity ( S<sub>CO</sub>, the ratio of CO to the sum of CO and CO<sub>2</sub> formed during the reaction ) was also calculated.

Tab 1 T<sub>i</sub> and S<sub>CO</sub> for catalysts

| Catalyst                                           | T <sub>i</sub> ( °C ) | S <sub>CO</sub> ( % ) |
|----------------------------------------------------|-----------------------|-----------------------|
| 1% Pt/SO <sub>2</sub>                              | 330                   | 0                     |
| SO <sub>2</sub>                                    | 480                   | 49                    |
| 0.02% Ir/SO <sub>2</sub>                           | 461                   | 9                     |
| 0.1% Ir/SO <sub>2</sub>                            | 421                   | 7                     |
| 1% Ir/SO <sub>2</sub>                              | 329                   | 6                     |
| 5% Ir/SO <sub>2</sub>                              | 315                   | 3                     |
| ZSM-5                                              | 471                   | 42                    |
| 0.02% Ir/ZSM-5                                     | 402                   | 5                     |
| 0.1% Ir/ZSM-5                                      | 377                   | 4                     |
| 1% Ir/ZSM-5                                        | 316                   | 4                     |
| 5% Ir/ZSM-5                                        | 302                   | 1                     |
| $\gamma$ -Al <sub>2</sub> O <sub>3</sub>           | 480                   | 37                    |
| 0.02% Ir/ $\gamma$ -Al <sub>2</sub> O <sub>3</sub> | 462                   | 9                     |
| 0.1% Ir/ $\gamma$ -Al <sub>2</sub> O <sub>3</sub>  | 445                   | 5                     |
| 1% Ir/ $\gamma$ -Al <sub>2</sub> O <sub>3</sub>    | 340                   | 4                     |
| 5% Ir/ $\gamma$ -Al <sub>2</sub> O <sub>3</sub>    | 321                   | 2                     |

Catalyst weight = 0.05 g, soot weight = 0.005 g, Feed gas composition = 420 ppm NO + 4.4% O<sub>2</sub> in He, flow rate = 100 ml/min.

### 3 Results and discussion

Table 1 showed the  $T_i$  and  $S_{CO}$  of a series of catalysts for soot oxidation. Compared the  $T_i$  and  $S_{CO}$  of 1% of Ir/SO<sub>2</sub> with that of 1% of Pt/SO<sub>2</sub>, we could see that the  $T_i$  of Ir/SO<sub>2</sub> was near to that of Pt/SO<sub>2</sub> but the  $S_{CO}$  of Ir/SO<sub>2</sub> was higher than that of Pt/SO<sub>2</sub>, which was in agreement with that reported by Wang et al<sup>[4]</sup>.

From the data on Ir/SO<sub>2</sub> that contained different Ir metal contents, we could see that, from blank SO<sub>2</sub> to 5% of Ir/SO<sub>2</sub>, the corresponding  $T_i$  was lowered and  $S_{CO}$  was decreased. On the samples supported with  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> or ZSM-5, the trend was agreement with that of Ir/SO<sub>2</sub>. This phenomena was similar to that reported by Xue et al<sup>[6]</sup>. In our work, although the correlation had not been established between the Ir content and the particle size, it seemed that the oxidation of soot and the selectivity to CO depended on the size of particles.

By comparing the  $T_i$  and  $S_{CO}$  in the same Ir content, the effect of support oxides was obtained. The data in the table show that the order of  $T_i$  was ZSM-5 < SO<sub>2</sub> <  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> and the order of  $S_{CO}$  was ZSM-5 <  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> < SO<sub>2</sub>. Xue et al<sup>[6]</sup> examined the effect of the support oxides on the oxidation of NO to NO<sub>2</sub> and found the catalytic activity order was Pt/SO<sub>2</sub> > Pt/ $\gamma$ -Al<sub>2</sub>O<sub>3</sub>. This result was similar to our results in the  $T_i$  of soot oxidation. The order of  $S_{CO}$  differed from the order of  $T_i$  was attributed to the interaction between  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> and NO<sub>2</sub> and the adsorption of NO<sub>2</sub> promoted the selectivity to CO<sub>2</sub>.

### 4 Conclusion

The soot oxidation with Ir-based catalysts was in-

vestigated using simulated diesel exhaust gases. Ir-based catalysts showed high catalytic activity for oxidation of soot and high CO selectivity in the presence of O<sub>2</sub> and NO. With the increasing of Ir content in the range examined (from zero to 5%), the catalytic activity increased and the CO selectivity decreased. Furthermore, support oxides had a little effect on the soot oxidation. The order of catalytic activity was Ir/ZSM-5 > Ir/SO<sub>2</sub> > Ir/ $\gamma$ -Al<sub>2</sub>O<sub>3</sub> and the order of selectivity to CO was Ir/ZSM-5 < Ir/ $\gamma$ -Al<sub>2</sub>O<sub>3</sub> < Ir/SO<sub>2</sub>.

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## 在 O<sub>2</sub> 和 NO 存在下 Ir 催化氧化黑烟的研究

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**摘要:** 模拟柴油机尾气中 O<sub>2</sub> 和 NO 的氛围, 研究了以 Ir 为基础的催化剂对黑烟的催化氧化。与 Pt/SO<sub>2</sub> 比较, Ir/SO<sub>2</sub> 对黑烟氧化有其相似的催化活性, 但有更高的 CO 选择性。通过测定 Ir 含量对催化活性和 CO 选择性的影响, 发现在研究的范围内 (0 到 5%), 随着 Ir 含量的增加, 催化活性增加, CO 选择性降低。此外, 测定了氧化物载体对催化活性及 CO 选择性的影响, 得到了催化活性顺序为 Ir/ZSM-5 > Ir/SO<sub>2</sub> > Ir/ $\gamma$ -Al<sub>2</sub>O<sub>3</sub>, CO 选择性顺序为 Ir/ZSM-5 < Ir/ $\gamma$ -Al<sub>2</sub>O<sub>3</sub> < Ir/SO<sub>2</sub>。

**关键词:** 黑烟氧化; Ir 催化剂; NO

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